

AD-A137 515

ANALYTICAL PREDICTION OF TURBULENT HEAT TRANSFER
PARAMETERS(U) COLORADO UNIV AT BOULDER DEPT OF
MECHANICAL ENGINEERING A BEJAN DEC 83 CUMER-83-4
RR02403-RR0240302 N00014-79-C-0006

1/1

UNCLASSIFIED

F/G 20/4

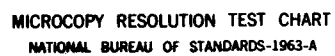
NL

END

FORMED

3+

BTIC



MICROCOPY RESOLUTION TEST CHART
NATIONAL BUREAU OF STANDARDS-1963-A

Analytical Prediction of Turbulent
Heat Transfer Parameters:

The Third Annual Report

Adrian Bejan

CUMER-83-4

December 1983

Analytical Prediction of Turbulent
Heat Transfer Parameters:

The Third Annual Report

Adrian Bejan

CUMER-83-4

December 1983



Unclassified

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER CUMER-83-4	2. GOVT ACCESSION NO. AD-A137515	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) Analytical Prediction of Turbulent Heat Transfer Parameters: The Third Annual Report		5. TYPE OF REPORT & PERIOD COVERED Annual 10/1/82 - 9/30/83
		6. PERFORMING ORG. REPORT NUMBER
7. AUTHOR(s) Adrian Bejan		8. CONTRACT OR GRANT NUMBER(s) N00014-79-C-0006
9. PERFORMING ORGANIZATION NAME AND ADDRESS Department of Mechanical Engineering, Campus Box 427, University of Colorado, Boulder, CO 80309		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS Program Element 61153N24 Project RR024-03, Task Area RR024-03-02, Work Unit NR09-43
11. CONTROLLING OFFICE NAME AND ADDRESS Office of Naval Research 800 N. Quincy Street Arlington, VA 22217		12. REPORT DATE December 1983
		13. NUMBER OF PAGES
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		15. SECURITY CLASS. (of this report)
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE
16. DISTRIBUTION STATEMENT (of this Report) Approved for public release; distribution unlimited		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report) Same as Block #16		
18. SUPPLEMENTARY NOTES		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) Heat transfer, turbulent flow, irreversibility, buckling theory.		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) The objective of this research is to construct a purely theoretical foundation for the phenomenon of turbulent heat transfer. In the present report it is shown that the buckling theory of inviscid streams and the classical hydrodynamic stability theory are in agreement with respect to the time scale criterion that accounts for transition to turbulence. Two experimental studies that confirm this correspondence are described.		

ANALYTICAL PREDICTION OF TURBULENT HEAT TRANSFER PARAMETERS:

THE THIRD ANNUAL REPORT

December 1983

Adrian Bejan
Associate Professor
Department of Mechanical Engineering
University of Colorado
Boulder, Colorado 80309

Prepared for

M. K. Ellingsworth
Program Monitor
The Office of Naval Research
Arlington, Virginia 22217



Accession For	
NTIS GRA&I	X
DTIC TAB	
Unannounced	
Justification	
By	
Distribution/	
Availability Codes	
Dist	Avail and/or Special
A-1	

Under Contract No. N00014-79-0006, Work Unit 097-431. Approved for public release; distribution unlimited. Reproduction in whole or in part is permitted for any purpose of the United States Government.

Background

This third annual report reviews the research produced by our group during the academic year 1982-1983, in the pursuit of a purely theoretical basis for turbulent flow phenomena and for performing engineering calculations of turbulent transport parameters. The objective of our work during the third year is better understood if one takes a brief look at our objectives and accomplishments during the first two years.

Our group's interest in the fundamentals of turbulent flow was sparked by the idea that any large-Reynolds-number stream (i.e., any stream that is relatively inviscid) possesses a longitudinal length scale (λ_B) which is proportional to the stream's transversal length scale (D). This longitudinal length scale is the widely observed meander wavelength of turbulent streams (jets, wakes, shear layers, plumes). The suggestion that " $\lambda_B/D = \text{constant}$ " is a property of all inviscid streams was published in 1981 as the end-result of the buckling theory of inviscid flow columns [1,2]. Whether or not the scaling law recommended by the buckling theory is correct remained to be established on the basis of old and new experiments. One issue we recognized from the start is that any theory that predicts a previously unknown property of turbulent flow deserves to be treated with serious attention, simply because turbulence science as we have it is dominated by empiricism. For this reason, any legitimate advance on the theoretical front is potentially capable of reducing significantly man's reliance on empiricism in dealing with engineering calculations of turbulent flow.

It is with this philosophical outlook that we devoted a good part of the last three years to the task of verifying the validity of the $\lambda_B \sim D$ scaling law of inviscid flow. During the first year we focused on a series of laboratory experiments designed to visualize the meandering or the buckling of high-Reynolds-number flows and to measure the λ_B/D constant. Another, much more rewarding phase

of our experimental effort was to sift through the fluid mechanics literature and to re-examine classical experimental results in light of our suspicion that beneath all of them resides the $\lambda_B \sim D$ property. We documented our experimental findings individually in the peer-refereed literature [3-5] and in review form in chapter 4 of my first book [6]. All the experiments examined by us - new and old - validate the buckling theory prediction that a longitudinal length scale exists, and that this length scale is proportional to the transversal length scale of the stream under consideration. It is worth pointing out that since its publication in 1981 the buckling theory has triggered at least one other experimental study [7], whose conclusions relative to the validity of the $\lambda_B \sim D$ scaling law is in perfect agreement with ours.

During the second year of this research program we turned our attention to analytical work that invokes the $\lambda_B \sim D$ property in order to predict some of the more frequently used features of turbulent flow. These analytical developments ranged from predicting the constant-angle growth (i.e., the triangular or conical shape) of all turbulent mixing regions, to calculating the viscous sublayer thickness in turbulent boundary layer flow. Samples of this analytical work are presented in the peer-refereed literature [6,8,9] and throughout the "turbulent flows" part of my course in convection heat transfer [10]. In all cases, the $\lambda_B \sim D$ property is used to derive analytically classical facts known empirically: this new property is used to partially replace empiricism with theory in our own comprehension of turbulence.

During the third year of sponsored research, 1982-1983, we could have continued with more buckling flow experiments and with more analyses of turbulent flow, and our success and productivity would have been assured. We chose not to do this (two years of intensive work of this kind were enough to satisfy our curiosity), instead, we devoted the third year to investigating the

possible relationship between buckling theory and hydrodynamic stability theory. We were able to show that the hydrodynamic stability theory of inviscid flow and the buckling theory of inviscid flow are in fact in agreement with regard to the existence of the $\lambda_B \sim D$ scaling law: as shown in the next section, the agreement between the two theories is easy to establish once "one knows what to look for" in the volume of information generated by hydrodynamic stability analyses, (i.e., once one knows from buckling theory that a certain proportionality of scales might have been overlooked).

Hydrodynamic stability theory and buckling theory vis-avis transition

A review of analytical results of linear stability analyses of inviscid flows (Table 1) shows that any inviscid stream of thickness D is unstable to disturbances whose longitudinal wavelength exceeds a certain multiple of D . For example, a two-dimensional inviscid jet of triangular profile is unstable to wavelengths in excess of $1.714 D$. Beginning with Rayleigh's paper [11], much has been made in the stability literature of the maximum exhibited by the growth rate of the disturbance. More interesting, however, is the "coincidence" that the neutral wavelength $1.714 D$ is only 5 percent smaller than the buckling wavelength scale of a two-dimensional stream ($\frac{\pi}{\sqrt{3}} D = 1.81 D$; see Refs. [1,6]). This coincidence seems to be insensitive to the actual shape of the $U(y)$ profile chosen for analysis. For example, in a stack of D -thick counterflow jets of sinusoidal profile ($u = U_0 \sin \pi y/D$) the neutral wavelength is $2 D$, which is only 10 percent greater than the buckling length scale ($\pi/\sqrt{3}$) D . The same scaling between flow thickness and neutral wavelength is revealed by the stability analysis of other finite-thickness flows (Table 1).

The proportionality of length scales identified in Table 1 tells us that during transition a stream can fluctuate relative to its ambient with a period

(a) free jet		$\lambda_{\min} = 1.714 D$
(b) shear layer		$\lambda_{\min} = 4.914 D$
(c) velocity discontinuity		$\lambda_{\min} = 0 \quad (D = 0)$

Table 1. Minimum wavelength for instability in inviscid flow

of order $\lambda/(U_0/2)$, where λ is the disturbance wavelength and U_0 the scale of the relative velocity between stream and ambient. And since for instability λ must be greater than a length nearly identical to the buckling wavelength λ_B [1,6], the stream fluctuation time scale will be equal to or greater than the buckling time

$$t_{\text{fluctuation}} \geq t_B = \frac{\lambda_B}{U_0/2} \quad (1)$$

Since $\lambda_B \sim D$, the fluctuation period exceeds a minimum value that is proportional to D . The same conclusion is shown graphically in Fig. 1: The domain of possible inviscid instability is situated to the right of the $t \sim D$ line represented by eq. (1).

Since "inviscidness" is a flow property, not a fluid property*, the domain of possible inviscid instability must also be situated to the left of the $t \sim D^2$ parabola on Fig. 1. The $t \sim D^2$ curve has its base in the argument that any stream (U_0, D) started impulsively relative to a stationary ambient becomes viscous during a time given by the scale of transversal viscous communication over a distance $D/2$ [1,6],

$$t_v = \frac{D^2}{16\nu} \quad (2)$$

Thus, the disturbed stream fluctuates as an inviscid stream if

$$t_{\text{fluctuation}} \leq t_v \quad (3)$$

*all fluids have a measurable viscosity, μ .

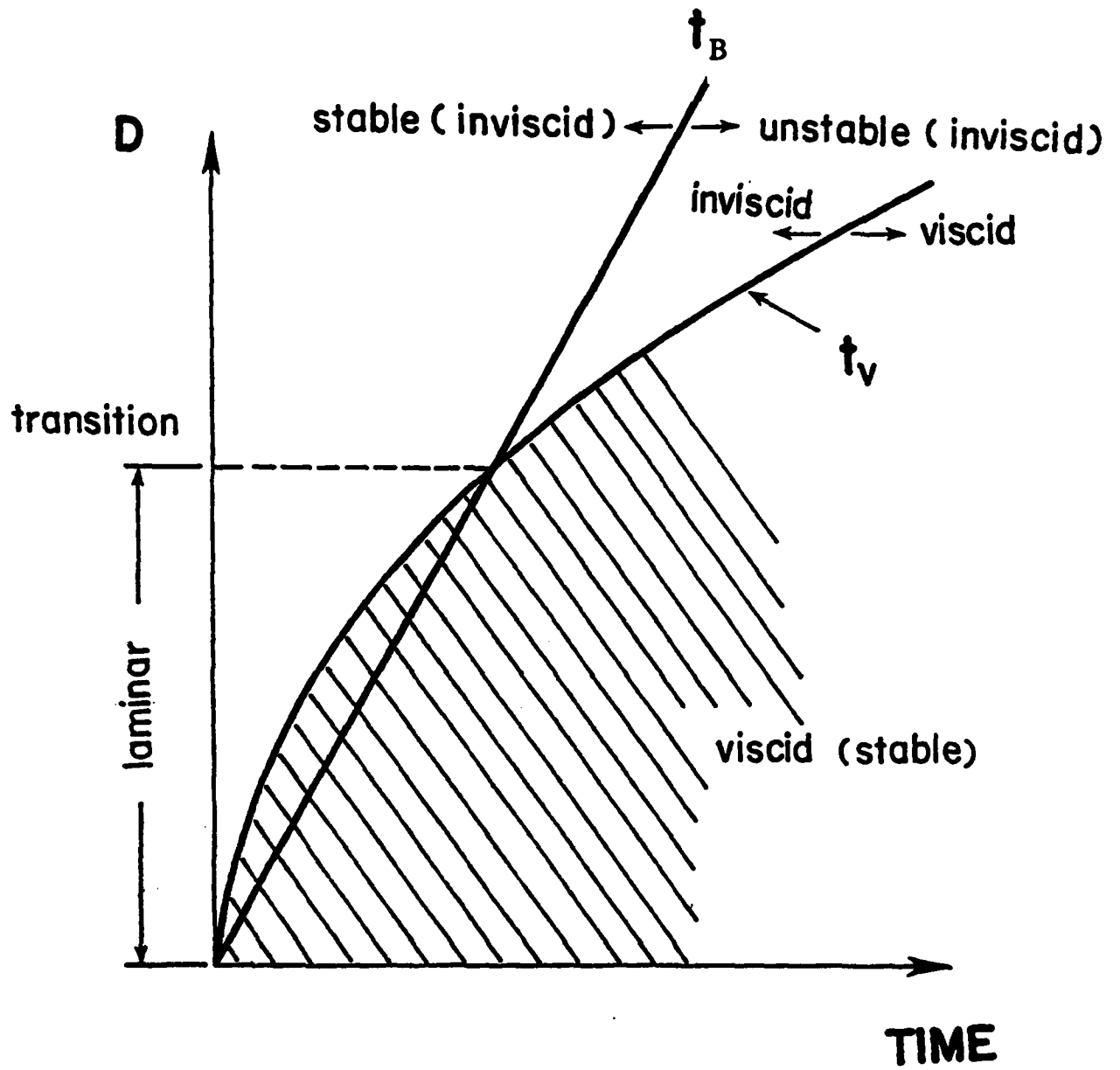


Figure 1

Combining eqs. (1) - (13), we learn that the transition is possible as long as

$$t_B \leq t_{\text{fluctuation}} \leq t_v . \quad (4)$$

Figure 1 suggests that in any stream-like flow the leading section of the flow is laminar, and that the transition is possible for the first time when the buckling number reaches $O(1)$,

$$N_B = \frac{t_v}{t_B} \sim 1 \quad (5)$$

In terms of a local Reynolds number based on local transversal length scale, $U_0 D / \nu$, the $N_B \sim 1$ criterion is written as

$$\frac{U_0 D}{\nu} \sim 10^2 . \quad (6)$$

The transition criterion (5,6), derived here based on the scaling trend discovered in some of the results of inviscid stability analyses (Table 1), is identical to the criterion suggested originally by the buckling theory of inviscid streams. Most recently, we tested this criterion against experiments on transition in round laminar plumes [12] and in natural convection boundary layers (wall jets) near vertical walls heated at uniform temperature or uniform heat flux [13]. These experiments are described next only in "abstract" form, as they have both been published in the peer-refereed literature^{*}.

^{*} reprints can be obtained by writing to Adrian Bejan, University of Colorado, Campus Box 427, Mechanical Engineering Department, Boulder, Colorado 80309

References

1. A. Bejan, "On the Buckling Property of Inviscid Jets and the Origin of Turbulence," Letters in Heat and Mass Transfer, Vol. 8, pp. 187-194, May-June 1981.
2. A. Bejan, "Comments on Viscous Buckling of Thin Fluid Layers," Physics of Fluids, Vol. 24, No. 9, pp. 1764, 1795, September 1981.
3. A. Bejan, "The Meandering Fall of Paper Ribbons, Physics of Fluids, Vol. 25, May, 1982, pp. 741,742.
4. M. G. Stockman and A. Bejan, "The Nonaxisymmetric (Buckling) Flow Regime of Fast Capillary Jets, Physics of Fluids, Vol. 25, September 1982, pp. 1506-1511.
5. A. Bejan, "Theoretical Explanation for the Incipient Formation of Meanders in Straight Rivers, Geophysical Research Letters, Vol. 9, August 1982, pp. 831-834.
6. A. Bejan, Entropy Generation Through Heat and Fluid Flow, John Wiley & Sons, New York, 1982.
7. A. Pollard, Private Communication,
Department of Mechanical Engineering, Queen's University, Kingston,
Ontario, Canada.
8. A. Bejan, Theory of Instantaneous Sinuous Structure in Turbulent Buoyant Plumes, Warme-und Stoffubertragung, Vol. 16, 1982, pp. 237-242.

9. R. Anderson and A. Bejan, "Buckling of a Turbulent Jet Surrounded by a Highly Flexible Duct," Physics of Fluids, Vol. 26, pp. 3193-3200, November 1983.
10. A. Bejan, Convection Heat Transfer, Wiley, New York, Chapters 6-8, 1984.
11. Lord Rayleigh, "On the Stability, or Instability of Certain Fluid Motions," Proc. Lon. Math. Soc., Vol. XI, 1880, pp. 57-70.
12. S. Kimura and A. Bejan, "Mechanism for Transition to Turbulence in Buoyant Plume Flow," Int. J. Heat Mass Transfer, Vol. 26, 1983, pp. 1515-1532.
13. A. Bejan and G. R. Cunnington, "Theoretical Considerations of Transition to Turbulence in Natural Convection Near a Vertical Wall," Int. J. Heat Flow, Vol. 4, 1983, pp. 131-139.

S. Kimura and A. Bejan, "Mechanism for Transition to Turbulence in Buoyant Plume Flow," Int. J. Heat Mass Transfer, Vol. 26, 1983, pp. 1515-1532.

Abstract

This paper reports a theoretical and experimental study of the fundamental mechanism responsible for transition in natural convection plume flow. Theoretically, it is argued that the transition occurs when the time of viscous penetration normal to the plume becomes comparable with the minimum time period with which the plume can fluctuate as an unstable inviscid stream. It is also argued that at transition the plume wavelength must always scale with the local plume diameter. The experimental part of the study focused on transition in the axisymmetric air plume above a point heat source. Smoke visualization of the plume shape at transition led to extensive observations that support strongly the transition mechanism proposed theoretically. The transitional plume is seen to meander in plane (two-dimensionally) and with a wavelength which scales with the plume diameter. If excited externally by many such wavelengths, the plume has the property to select the natural wavelength proposed theoretically. The equivalence between the present transition mechanism and the transition predicted by the buckling theory is discussed.

A. Bejan and G. R. Cunnington, "Theoretical Considerations of Transition to Turbulence in Natural Convection Near a Vertical Wall," Int. J. Heat Fluid Flow, Vol. 4, 1983, pp. 131-139.

Abstract

Hydrodynamic stability analysis of an inviscid wall jet shows that instability is possible above a characteristic disturbance wavelength which is proportional to the jet thickness. This scaling is the basis for an argument that transition occurs when the fluctuating time period of the unstable (inviscid) wall jet is of the same order as the viscous diffusion time normal to the jet. The transition must occur when the Jet Reynolds number is of the order of 10^2 . Published observations of transition along a heated vertical wall are reviewed in order to test the validity of the proposed scaling argument. Specifically, numerous observations on buoyant jets near isothermal walls, near constant-heat-flux walls, and in enclosures with vertical isothermal walls are shown to support the validity of the transition mechanism proposed.

Summary of Student Theses

1. "Entropy Generation Criterion Applied to Various Heat Transfer Augmentation Techniques," by William Robert Ouellette, 1979; M.S. Thesis.
2. "Extended Surface Design of Minimum Irreversibility," by Dimosthenis Poulikakos, 1980; M.S. Thesis.
3. "The Buckling Instability of Capillary Jets," by Michael Geoffrey Stockman, 1981; M.S. Thesis.
4. "Viscous Buckling of Thin Fluid Layers Undergoing End Compression," by Kenneth R. Blake, 1982; M.S. Thesis.
5. "Buckling of Turbulent Jets," by Ren Scott Anderson, May 1983; Ph.D. Thesis.
6. "Buckling Flow and Transition to Turbulence in Axisymmetric Plumes," by Shigeo Kimura, May 1983; Ph.D. Thesis.
7. "Transition to Turbulence in Rivulet Flow between Two Parallel Plates," by Anil Anand, 1983; M.S. Thesis.

DISTRIBUTION LIST

HEAT TRANSFER

One Copy except
as noted

Mr. M. Keith Ellingsworth
Mechanics Division
Office of Naval Research
800 N. Quincy Street
Arlington, VA 22203

2

Defense Documentation Center
Building 5, Cameron Station
Alexandria, VA 22314

12

Technical Information Division
Naval Research Laboratory
4555 Overlook Avenue SW
Washington, DC 20375

6

Professor Paul Marto
Department of Mechanical Engineering
U.S. Naval Post Graduate School
Monterey, CA 93940

Professor Bruce Rankin
Naval Systems Engineering
US Naval Academy
Annapolis, MD 21402

Mr. Doug Marron
Code 05R13
Crystal Plaza # 6
Naval Sea Systems Command
Washington, DC 20362

Steam Generators Branch, Code 5222
National Center #4
Naval Sea Systems Command
Washington, D.C. 20362

Heat Exchanger Branch, Code 5223
National Center #3
Naval Sea Systems Command
Washington, D.C. 20362

Mr. Ed Ruggiero, NAVSEA 08
National Center #2
Washington, D.C. 20362

Dr. Earl Quandt Jr., Code 272
David Taylor Naval Ship R&D Center
Annapolis, MD 21402

Mr. Wayne Adamson, Code 2722
David Taylor Naval Ship R&D Center
Annapolis, MD 21302

Dr. Win Aung
Heat Transfer Program
National Science Foundation
Washington, DC 20550

Mr. Michael Perlsweig
Department of Energy
Mail Station E-178
Washington, DC 20545

Dr. W.H. Theilbahr
Chief, Energy Conservation Branch
Dept. of Energy, Idaho Operations Office
550 Second Street
Idaho Falls, Idaho 83401

Professor Ephriam M. Sparrow
Department of Mechanical Engineering
University of Minnesota
Minneapolis, MN 55455

Professor S.V. Patankar
Department of Mechanical Engineering
University of Minnesota
Minneapolis, MN 55455

Professor Daryl Metzger
Chairman, Mechanical and
Energy Systems Engineering
Arizona State University
Tempe, AZ 85281

Professor Ronald So
Mechanical and Energy Systems
Engineering
Arizona State University
Tempe, AZ 85281

Professor J.A.C. Humphrey
Department of Mechanical Engineering
University of California, Berkeley
Berkeley, CA 94720

Professor Brian Launder
Thermodynamics and Fluid Mechanics Division
University of Manchester
Institute of Science & Technology
PO88 Sackville Street
Mandhester M601QD England

Professor Shi-Chume Yao
Department of Mechanical Engineering
Carnegie-Mellon University
Pittsburgh, PA 15213

Professor Charles B. Watkins
Chairman, Mechanical Engineering Department
Howard University
Washington, DC 20059

Professor Adrian Bejan
Department of Mechanical Engineering
University of Colorado
Boulder, CO 80309

Professor Donald M. McEligot
Department of Aerospace and Mechanical Engineering
Engineering Experiment Station
University of Arizona
Tucson, Arizona 85721

Professor Paul A. Libby
Department of Applied Mechanics and Engineering Sciences
University of California San Diego
Post Office Box 109
La Jolla, CA 92037

Professor C. Forbes Dewey, Jr.
Fluid Mechanics Laboratory
Massachusetts Institute of Technology
Cambridge, MA 02139

Professor William G. Characklis
Dept. of Civil Engineering and Engineering Mechanics
Montana State University
Bozeman, MT 59717

Professor Ralph Webb
Department of Mechanical Engineering
Pennsylvania State University
208 Mechanical Engineering Bldg.
University Park, PA 16802

Professor Warren Rohsenow
Mechanical Engineering Department
Massachusetts Institute of Technology
77 Massachusetts Avenue
Cambridge, MASS 02139

Professor A. Louis London
Mechanical Engineering Department
Bldg. 500, Room 501B
Stanford University
Stanford, CA 94305

Professor James G. Knudsen
Associate Dean, School of Engineering
Oregon State University
219 Covell Hall
Corvallis, Oregon 97331

Professor Arthur E. Bergles
Mechanical Engineering Department
Iowa State University
Ames, Iowa 50011

Professor Kenneth J. Bell
School of Chemical Engineering
Oklahoma State University
Stillwater, Oklahoma 74074

Dr. James Lorenz
Componebt Technology Division
Argonne National Laboratory
9700 South Cass Avenue
Argonne, Illinois 60439

Dr. David M. Eissenberg
Oak Ridge National Laboratory
P.O. Box Y, Bldg. 9204-1, MS-0
Oak Ridge, Tennessee 37830

Dr. Jerry Taborek
Technical Director
Heat Transfer Research Institute
1000 South Fremont Avenue
Alhambra, CA 91802

Dr. Simion Kuo
Chief, Energy Systems
Energy Research Laboratory
United Technology Research Center
East Hartford, CT 06108

Mr. Jack Yampolsky
General Atomic Company
P.O. Box 81608
San Diego, CA 92138

Mr. Ted Carnavos
Noranda Metal Industries, Inc.
Prospect Drive
Newton, CONN 06470

Dr. Ramesh K. Shah
Harrison Radiator Division
General Motors Corporation
Lockport, New York 14094

Dr. Ravi K. Sakhuja
Manager, Advanced Programs
Thermo Electron Corporation
101 First Avenue
Waltham, MASS 02154

Mr. Robert W. Perkins
Turbotec Products, Inc.
533 Downey Drive
New Britain, CONN 06051

Dr. Keith E. Starner
York Division, Borg-Warner Corp.
P.O. Box 1592
York, PA 17405

Mr. Peter Wishart
C-E Power Systems
Combustion Engineering, Inc.
Windsor, CONN 06095

Mr. Henry W. Braum
Manager, Condenser Engineering Department
Delaval
Front Street
Florence, New Jersey 08518

Dr. Thomas Rabas
Steam Turbine-Generator Technical Operations Division
Westinghouse Electric Corporation
Lester Branch
P.O. Box 9175 N2
Philadelphia, PA 19113

END

FILMED

3-84

DTIC